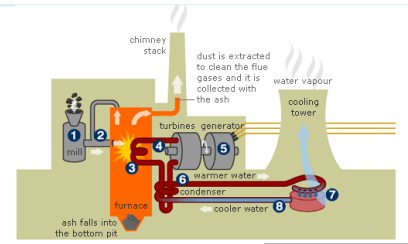


Heat Engines (p118)

Q1: A steam-cycle power station has a boiler temperature of 520°C and a condensor temperature of 21°C.
What is the maximum (theoretical) efficiency? (%)



Max theoretical efficiency = ideal = Carnot

Carnot efficiency: (Ideal efficiency)

$$\eta_c = 1 - \frac{T_c}{T_h}$$

where

T_h = the hot temperature (Kelvin) that the heat flows FROM

T_c = the cold temperature (Kelvin) that the heat flows TO

$$T_h = 520 + 273 = 793 \text{ K}$$

$$T_c = 21 + 273 = 294 \text{ K}$$

$$n = 1 - 294/793 = 0.6293 \text{ (63\%)}$$

More likely $T_2 = 150$

$$T_c = 273 + 150 = 423$$

$$n = 1 - 423/795 = 0.4679 \text{ (47\%)}$$

Q3: Solar powered Stirling Engine: A mirror of diam 12 m focusses sunlight (599 W/m²) to achieve maximum temperature of 717°C. Air is at 21°C.

(a) Find theoretical efficiency (%)

$$\eta_c = 1 - \frac{T_c}{T_h}$$

$$\begin{aligned} \text{Theoretical eff} &= 1 - (273 + 21) / (273 + 717) \\ &= 0.703 \text{ (70.3\%)} \end{aligned}$$



(b) Find heat supply rate.

Heat from sun = Area of mirror * heat from sun

$$= \pi * 6^2 * 599$$

$$= 113.097 * 599 = 67745 \text{ W}$$

(c) Find theoretical power output.

Work Output = Heat Supplied - Heat Rejected

$$W = Q_s - Q_R$$

So efficiency

$$\eta = W / Q_s, \text{ So } W = \eta Q$$

$$= 0.703 * 67745 = 47624.735 \text{ W}$$

Internal Combustion

Thursday, 17 November 2011
12:30 PM

Q6: An internal combustion engine uses fuel with energy content of 37.1 MJ/kg at a rate of 4.2 kg/hour. Efficiency is 30%.

(a) What is the power output?

Heat supplied: $Q_s = mE$

$m = \text{mass/sec}$

$$= 4.2/3.600 = 1.1667 \text{ E-3 kg/s}$$

$$Q_s = 1.1667\text{E-3} \times 37.1\text{E6} = 43284.57 \text{ J/s (W)}$$

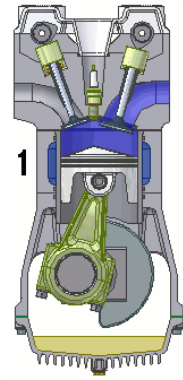
$$W = \eta Q$$

$$= 0.30 \times 43284.57 = 12985.4 \text{ Joules/s (W)}$$

(b) What is the rate of heat generated?

$$Q_s = W + Q_R$$

$$Q_R = Q_s - W = 43284.57 - 12985.4 = 30299.17 \text{ J/s (W)}$$



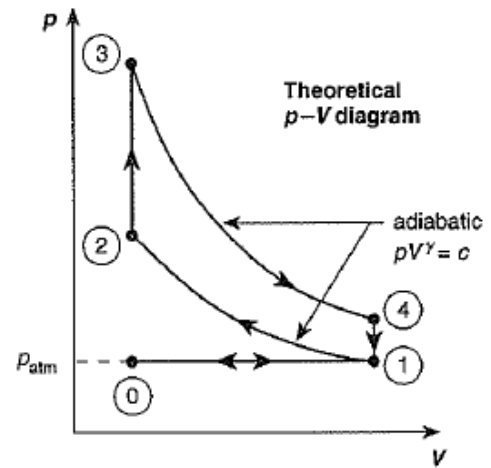
Otto Cycle P-V

Thursday, 17 November 2011

12:50 PM

Q8: Otto cycle; Compression ratio = 8.3:1, inlet = 96.8kPa (abs) at 54°C. Heat supply = 945 kJ/kg of air.

(a) Find compression temperature T2 (K).



Note: This question is worked out for each **kg** of air. (specific power)

Identify the gas process.

Adiabatic compression

$$pV^n = \text{constant}$$

$$\frac{T_2}{T_1} = \left(\frac{V_1}{V_2}\right)^{n-1}$$

$$\frac{p_2}{p_1} = \left(\frac{T_2}{T_1}\right)^{\frac{n}{n-1}}$$

Convert:

$$T_1 = 54 + 273.15 = 327.15 \text{ K}$$

$$(V_1/V_2) = \text{compression ratio} = 8.3$$

$$T_2 = T_1 \cdot (V_1/V_2)^{n-1}$$

$$T_2 = 327.15 \cdot 8.3^{(1.4-1)} = 762.743 \text{ K (490 °C)}$$

And... for fun...

$$P_2 = P_1 \cdot (T_2/T_1)^{n/(n-1)}$$

$$= 96800 \cdot (762.743/327.15)^{(1.4/0.4)}$$

$$= 1.8732\text{E}6 \text{ Pa}$$

Process	Relationship between p, V, T	Work (W)	Internal-energy change ($U_2 - U_1$)	Heat (Q)
constant pressure	$p = \text{constant}$ $\frac{V_1}{T_1} = \frac{V_2}{T_2}$	$p(V_2 - V_1)$	$mc_v(T_2 - T_1)$	$mc_p(T_2 - T_1)$
constant volume	$V = \text{constant}$ $\frac{p_1}{T_1} = \frac{p_2}{T_2}$	0	$mc_v(T_2 - T_1)$	$Q = U_2 - U_1$ $Q = mc_v(T_2 - T_1)$
isothermal	$T = c$ $p_1V_1 = p_2V_2$	$p_1V_1 \ln \left(\frac{V_2}{V_1}\right)$	0	$Q = W$ $Q = p_1V_1 \ln \left(\frac{V_2}{V_1}\right)$
polytropic	$pV^n = \text{constant}$ $\frac{T_2}{T_1} = \left(\frac{V_1}{V_2}\right)^{n-1}$ $\frac{p_2}{p_1} = \left(\frac{T_2}{T_1}\right)^{\frac{n}{n-1}}$	$\frac{p_1V_1 - p_2V_2}{n-1}$	$mc_v(T_2 - T_1)$	$Q = W + U_2 - U_1$
adiabatic	as for polytropic with $n = \gamma$	as for polytropic with $n = \gamma$	$mc_v(T_2 - T_1)$	0

(b) Find maximum temperature T3 (K).

Identify the gas process. Constant volume heating (Isochoric)

$$Q = mc_v(T_3 - T_2)$$

$$T_3 = T_2 + Q / mc_v$$

$$= 762.743 + 945000 / (1 \cdot 718)$$

$$= 2078.9 \text{ K}$$

$$P_3 = P_2 \cdot T_3/T_2$$

$$= 1.8732\text{E}6 \cdot 2078.9/762.743$$

$$= 5.1055\text{E}6 \text{ Pa}$$

Gas	Formula	c_p Constant Pressure Specific Heat Capacity (kJ/kgK) at 20°C	c_v Constant Volume Specific Heat Capacity (kJ/kgK) at 20°C
Acetone		1.47	1.32
Acetylene	C_2H_2	1.69	1.37

$$= 5.1055 \text{E}6 \text{ Pa}$$

Acetone		1.47	1.32
Acetylene	C_2H_2	1.69	1.37
Air		1.005	0.718

Q10: (cont) Otto cycle; Compression ratio = 8.3:1, inlet = 96.8kPa (abs) at 54°C. Heat supply = 945 kJ/kg of air.
(c) Find expanded temperature T4 (K).

Adiabatic expansion...

$$T_4 = T_3 \cdot (V_3/V_4)^{(n-1)}$$

Expansion ratio

$$1/8.3 = 0.1205$$

$$T_3 = 2078.899 \text{ K}$$

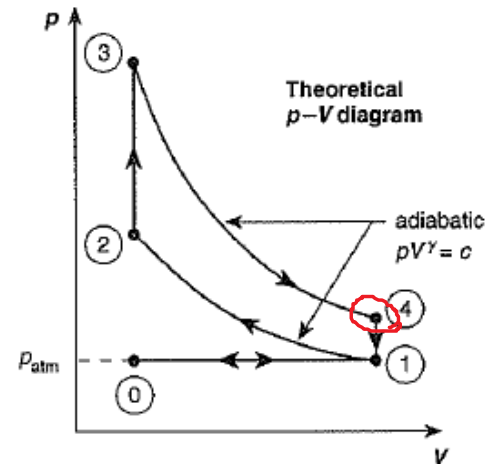
So...

$$\begin{aligned} T_4 &= T_3 \cdot (V_3/V_4)^{(n-1)} \\ &= 2078.899 \cdot 0.1205^{0.4} \\ &= 891.7194 \text{ K} \end{aligned}$$

and... (for fun)

$$\begin{aligned} P_4 &= P_3 \cdot (T_4/T_3)^{(n/(n-1))} \\ &= 5.1055 \text{E}6 \cdot (891.7194/2078.9)^{(1.4/0.4)} \\ &= 263888 \text{ Pa} \end{aligned}$$

$$\begin{aligned} pV^n &= \text{constant} \\ \frac{T_2}{T_1} &= \left(\frac{V_1}{V_2} \right)^{n-1} \\ \frac{p_2}{p_1} &= \left(\frac{T_2}{T_1} \right)^{\frac{n}{n-1}} \end{aligned}$$



Q11: (cont) Otto cycle; Compression ratio = 8.3:1, inlet = 96.8kPa (abs) at 54°C. Heat supply = 945 kJ/kg of air.
(d) Find indicated work (per kg of air).

Indicated power (no friction losses)

Power = Work/sec

$$W_{\text{Indicated}} = W_{\text{Expand}} - W_{\text{Compress}}$$

$$W_{\text{Expand}} = \frac{p_3 V_3 - p_4 V_4}{n-1}$$

But we don't know the VOLUME!

(See example p137-138)

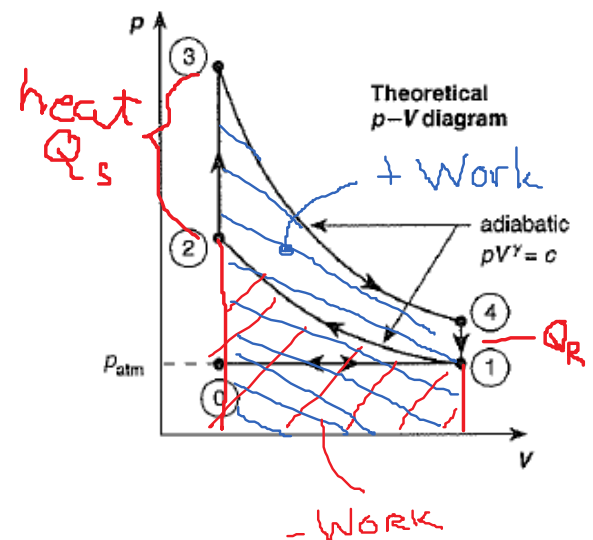
Use heat rejected...

$$W = Q_S - Q_R$$

Q_S = heat gain from 2 to 3 (const volume)

$Q = 945000 \text{ J/kg}$ (from fuel)

Q_R = heat loss from 4 to 1



polytropic	$pV^n = \text{constant}$ $\frac{T_2}{T_1} = \left(\frac{V_1}{V_2} \right)^{n-1}$ $\frac{p_2}{p_1} = \left(\frac{T_2}{T_1} \right)^{\frac{n}{n-1}}$	$\frac{p_1 V_1 - p_2 V_2}{n-1}$
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$$\dot{Q} = 945000 \text{ J/kg (from fuel)}$$

\dot{Q}_R = heat loss from 4 to 1

$$\begin{aligned}\dot{Q}_R &= m c_v (T_1 - T_4) \\ &= 1 * 718 * (327.15 - 891.7194) \\ &= -405361 \text{ J/kg}\end{aligned}$$

$$\begin{aligned}W &= \dot{Q}_S - \dot{Q}_R \\ &= 945000 - 405361 \\ &= 539639 \text{ J/kg}\end{aligned}$$

(e) Find theoretical efficiency (%).

$$\eta = 1 - \frac{\dot{Q}_R}{\dot{Q}_S} = 1 - \frac{\dot{Q}_R}{\dot{Q}_S}$$

$$\begin{aligned}\eta &= 1 - \dot{Q}_R / \dot{Q}_S \\ &= 1 - (405361 / 945000) = 0.571\end{aligned}$$

or...

$$\eta = W / \dot{Q}_S = 539639 / 945000 = 0.571$$

	$\frac{p_2}{p_1} = \left(\frac{T_2}{T_1}\right)^{\frac{n}{n-1}}$	
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Steam Engine

Thursday, 17 November 2011
1:45 PM

Q16: A steam engine outputs 54 kW using wood (energy content 19.8 MJ/kg) at a rate of 25 kg/hour. Steam is at 520°C and cooling water is at 20°C . (a) What is the overall efficiency? (%)

$$\eta = \frac{W}{Q_s}$$

$$Q_s = mE$$

Q17: (cont) A steam engine outputs 54 kW using wood (energy content 19.8 MJ/kg) at a rate of 25 kg/hour. Steam is at 520°C and cooling water is at 20°C . (b) Find the maximum (theoretical) efficiency. (%)

Max theoretical efficiency = ideal = Carnot

Carnot efficiency: (Ideal efficiency)

$$\eta_c = 1 - \frac{T_c}{T_h}$$

where

T_h = the hot temperature (Kelvin) that the heat flows FROM

T_c = the cold temperature (Kelvin) that the heat flows TO

Ocean Thermal

Thursday, 17 November 2011
1:55 PM

Q18: OTEC: Power output = 1.08 MW, $T_2 = 23.1^\circ\text{C}$, $T_1 = 9.25^\circ\text{C}$. The overall plant efficiency is 44% of Carnot %.
(a) Find Carnot efficiency (%). (Hint: For the working fluid, the heat exchangers miss by 3 degrees!)

$$\eta_C = 1 - \frac{T_c}{T_h}$$

Find temperatures of the Working Fluid. (Ammonia)

(This is not a gas, so we don't need to use gas process equations)

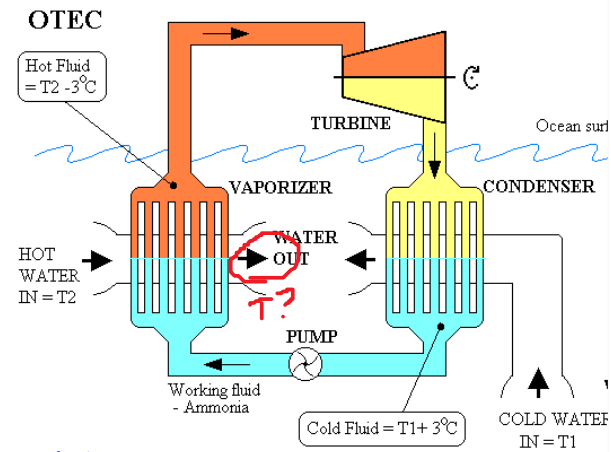
$$T_C = 273 + (9.25 + 3) = 285.25 \text{ K}$$

$$T_H = 273 + (23.1 - 3) = 293.1 \text{ K}$$

$$\eta = 1 - 285.25/293.1 = 0.0268 \text{ (2.68\%)}$$

$$0.44 * 2.68 = 1.1792 \text{ (0.011792)}$$

Ocean Thermal Energy Conversion (OTEC)



Find the heat supply rate...

W , η , \dot{Q}_s
↓ ✓ ?

From ... $W = \eta \dot{Q}_s$ (now find \dot{Q}_s)...

$$\begin{aligned} \dot{Q}_s &= W/\eta \\ &= 1.08 * 1000000 / 0.011792 \\ &= 91646786 \text{ W (91.6 MW... Wow!)} \end{aligned}$$

Find hot seawater flow rate. (kg/s)

The hot seawater heats the ammonia up to within 3° of the hot incoming seawater temperature. That means the seawater itself is cooled down by 3 degrees by the time it comes out of that heat exchanger. (This assumes both fluids exit the heat exchanger at the same temperature - which is

approximately correct here - not that we are told anything else anyway, so we have to assume it in this case.)

$$\text{From } \dot{Q} = \dot{m}c\Delta T$$

$$\text{then } \dot{m} = \dot{Q}/(c\Delta T)$$

$$= 91646786/(4*1000*3)$$

$$= 7637.23 \text{ kg/s (7.6 tonnes per sec!)}$$

Find heat rejection rate.

$$W = Q_s - Q_R$$

Simply take away the work from the supplied heat. (We can also do this in rate - per second - format too)

$$Q_R = Q_s - W$$

$$= 91646786 - 1080000$$

$$= 90566786 \text{ W (90.5 MW)}$$

Find cold seawater flow rate. (kg/s).

Same as the hot water (heat source), the cold seawater (heat rejector) cools the ammonia down to within 3° of the cold incoming seawater temperature. That means the seawater itself is heated up by 3 degrees by the time it comes out of that heat exchanger. (Assuming both fluids exit the heat exchanger at the same temperature again)

$$\text{From } \dot{Q} = \dot{m}c\Delta T$$

$$\text{then } \dot{m} = \dot{Q}/(c\Delta T)$$

$$= 90566786/(4*1000*3)$$

$$= 7547.23 \text{ kg/s (7.5 tonnes per sec!)}$$

